

#### **PLEASE NOTE:**

The information contained in this document was obtained from sources believed to be reliable and is based on technical information and experience currently available from members of the Compressed Gas Association, Inc. and others. However, the Association or its members, jointly or severally, make no guarantee of the results and assume no liability or responsibility in connection with the information or suggestions herein contained. Moreover, it should not be assumed that every acceptable commodity grade, test or safety procedure or method, precaution, equipment or device is contained within, or that abnormal or unusual circumstances may not warrant or suggest further requirements or additional procedure.

This document is subject to periodic review, and users are cautioned to obtain the latest edition. The Association invites comments and suggestions for consideration. In connection with such review, any such comments or suggestions will be fully reviewed by the Association after giving the party, upon request, a reasonable opportunity to be heard. Proposed changes may be submitted via the Internet at our website, <a href="https://www.cganet.com">www.cganet.com</a>.

This document should not be confused with federal, state, provincial, or municipal specifications or regulations; insurance requirements; or national safety codes. While the Association recommends reference to or use of this document by government agencies and others, this document is purely voluntary and not binding unless adopted by reference in regulations.

A listing of all publications, audiovisual programs, safety and technical bulletins, and safety posters is available via the Internet at our website at <a href="www.cganet.com">www.cganet.com</a>. For more information contact CGA at Phone: 703-788-2700, ext. 799. E-mail: <a href="customerservice@cganet.com">customerservice@cganet.com</a>.

Work Item 08-044 Atmospheric Gases and Equipment Committee

NOTE—Technical changes from the previous edition are underlined.

FIFTH EDITION: 2013 FOURTH EDITION: 2005 REAFFIRMED: 1994, 2002 THIRD EDITION: 1989

© 2013 The Compressed Gas Association, Inc. All rights reserved.

All materials contained in this work are protected by United States and international copyright laws. No part of this work may be reproduced or transmitted in any form or by any means, electronic or mechanical including photocopying, recording, or any information storage and retrieval system without permission in writing from The Compressed Gas Association, Inc. All requests for permission to reproduce material from this work should be directed to The Compressed Gas Association, Inc., 14501 George Carter Way, Suite 103, Chantilly VA 20151. You may not alter or remove any trademark, copyright or other notice from this work.

Co	ntents		Page				
1	Introd	luction	1				
2	Scope	Scope					
3	Typic	al ASU features	1				
4	Defin	Definitions					
5	Healt	h hazards	7				
Ü	5.1	Cryogenic liquids					
	5.2	Gas products					
	5.3	Asphyxiation					
	5.4	Oxygen hazards					
	5.5	Protective clothing and personal protective equipment	9				
6	Gene	General plant considerations1					
	6.1	Site selection					
	6.2	Safety factors in plant layouts					
	6.3	Materials of construction					
	6.4	Insulation—other than coldbox					
	6.5	Cleaning					
	6.6	Electrical requirements					
	6.7	Noise					
7		e air quality					
	7.1	Contaminants					
	7.2 7.3	Reactive contaminants that concentrate in oxygen					
	7.3 7.4	Reactive contaminants that concentrate in nitrogen  Plugging components					
	7. <del>4</del> 7.5	Haze and smoke from fires					
	7.6	Contaminant sources.					
	7.7	Identification of contaminants					
	7.8	Location of air intake					
	7.9	Monitoring intake air					
8	Comr	Compressors					
	8.1	Axial compressors					
	8.2	Centrifugal compressors					
	8.3	Other dynamic compressor considerations	18				
	8.4	Reciprocating compressors					
	8.5	Diaphragm compressors					
	8.6	Rotary positive displacement compressors					
	8.7	Refrigerant gas compressors					
	8.8	Screw compressors					
	8.9	Lubrication systems					
	8.10	Coolers and separators					
	8.11 8.12	Suction filters or screens					
	8.13	Operating and maintenance procedures					
9	Δir oc	ontaminant removal	24				
	9.1	Removal methods					
	9.2	Contaminant removal stages					
	9.3	Prepurification unit operation					
	9.4	REVEX operation					
	9.5	Supplemental mechanical chillers					
	9.6	Caustic scrubbers					

10		ders			
	10.1	Loss of loading and overspeed			
	10.2	Oil contamination of the process			
	10.3	Abnormally low temperatures			
	10.4	Solids in gas stream	. 34		
	10.5	Loss of lubrication			
	10.6	Abnormal bearing temperature	. 35		
	10.7	Abnormal vibration			
	10.8	Abnormal speed			
		Critical speed	. 35		
		Fouling of expander with ice or carbon dioxide			
		Startup and shutdown			
		Operating and maintenance procedures			
		operating and manter are processed on the second of the se			
11	Cryog	enic pumps	. 36		
	11.1	General	. 36		
	11.2	Types of pumps	. 37		
	11.3	Materials of construction			
	11.4	Pump system design			
	11.5	Special considerations for oxygen service			
	11.6	Pump motor			
	11.7	Pump operation			
	11.8	Operating and maintenance procedures			
12	Coldb	XCXC			
	12.1	Removing particulate material			
	12.2	Cryogenic adsorbers			
	12.3	Liquid levels	.41		
	12.4	Monitoring contaminants	. 42		
	12.5	Argon separation and purification	. 42		
	12.6	Noncondensable purge			
	12.7	Coldbox cleaning			
	12.8	Safe holding time for LOX			
	12.9	Liquefaction of air in the main heat exchanger			
	12.10	Process upsets			
40					
13		ol systems			
	13.1	Instrumented systems functions			
		Critical safety systems			
		Operational safety systems			
	13.4				
		Unattended or partially attended operation			
	13.6	Remote operation	. 48		
	13.7	Additional considerations for computer-based control systems			
	13.8	Additional considerations for failsafe systems			
	13.9	Alarm system			
	13.10	Regulatory considerations	. 50		
11	Product handling equipment				
14					
	14.1	Light arrest and storage			
	14.2	High pressure gas storage vessels			
	14.3	Liquid vaporizers	. ე		
15	Coolin	g systems	. 52		
16		piping			
	16.1	General design considerations for plant piping			
	16.2	General design considerations for check valves			
	16.3	Oxygen piping hazards	. 50		

	16.4	Pressure relief devices	53	
	16.5	Cryogenic piping	54	
	16.6	Dead legs	54	
	16.7	Carbon steel piping	55	
	16.8	Venting	55	
	16.9	Product delivery		
17	Shutd	lown procedures	56	
	17.1	Coldbox shutdown		
	17.2	Liquid and gas disposal		
	17.3	Plant derime		
18	Repai	ir and inspection	57	
. •	18.1	General maintenance considerations		
	18.2	Supervisory control		
	18.3	Special construction and repair considerations		
	18.4	Coldbox hazards		
	18.5	Hazards of working in oxygen-enriched or oxygen-deficient atmospheres		
	18.6	Cleaning		
19	Operations and training			
	19.1	Operating procedures		
	19.2	Commissioning procedures		
	19.3	Emergency procedures		
	19.4	Management of change		
	19.5	Personnel training		
20	Refer	ences	61	
Fig	ure			
Fig	ure 1—	-Representative air separation plant flow diagram	2	
Tak	les			
Tab	le 1—	Effects at various oxygen breathing levels	9	
		Plugging, reactive, and corrosive contaminants in air		
		Typical default air quality design basis		
		Typical removal in PPU process		
		Typical removal in REVEX process		
ıah	16 K-	Cryogenic adsorber names	40	

## 1 Introduction

This publication provides guidance on the safe operation of cryogenic air separation plants. It is based on the experience of CGA member companies that operate cryogenic air separation units (ASUs).

Industrial cryogenic air separation has some potential hazards that must be recognized and addressed. The hazards include electricity, gases under pressure, very low temperatures, the ability of oxygen to accelerate combustion, and the asphyxiant properties of nitrogen, argon, and the rare gases [1].

Cryogenic air separation technology is not static; it has been progressing for decades and will continue to do so because of engineering development efforts. Consequently, plant process cycles, equipment, and operating conditions can be and are of varying kinds. Therefore, this publication must include generalized statements and recommendations on matters for which there is a diversity of opinion or practice. Users of this guide should recognize that it is presented with the understanding that it cannot take the place of sound engineering judgment, training, and experience. It does not constitute, and should not be construed to be, a code of rules or regulations.

# 2 Scope

This publication serves the interest of those associated or concerned with air separation plant operations and applies to safety in the design, location, construction, installation, operation, and maintenance of cryogenic air separation plants. Emphasis is placed on equipment and operational and maintenance features that are peculiar to cryogenic air separation processes. Limited coverage is given to plant equipment such as air compressors, which are used in other industrial applications and for which safe practices in design, installation, and use have already been established elsewhere. Further, as this publication is not intended as a universal safe practice manual for specific design and safety features, it is also important to refer to the operating manuals of the equipment suppliers.

The following are excluded from this publication:

- cylinder filling facilities;
- rare gas purification <u>systems</u>; and
- product transmission piping outside the plant boundaries.

# 3 Typical ASU features

Cryogenic ASUs have these features:

- air compression;
- air contaminant removal;
- heat exchange;
- distillation; and
- expansion (or other refrigeration sources).

Figure 1 is an example of a flow diagram for separating air by cryogenic distillation producing oxygen, nitrogen, and argon products. Air is compressed in the main air compressor (MAC) to between 4 atm and 10 atm. It is then cooled to ambient temperature. Trace contaminants such as water, carbon dioxide, and heavy hydrocarbons are removed <u>using systems such as a prepurification unit (PPU)</u> or a reversing heat exchanger (REVEX). The main heat exchanger cools the air to near its liquefaction temperature before entering the high pressure (HP) distillation column. Some of the air is reduced in pressure in the expander to produce refrigeration, overcoming heat leak and process inefficiencies. Gaseous nitrogen from the top of the HP column

This is a preview. Click here to purchase the full publication.

<sup>&</sup>lt;sup>1</sup> References are shown by bracketed numbers and are listed in order of appearance in the reference section.

is condensed by the reboiler and the liquid used to reflux both columns. Condensing nitrogen releases heat to vaporize liquid oxygen (LOX) in the low pressure (LP) column sump, which is then taken as product or sent as stripping gas to the LP column.

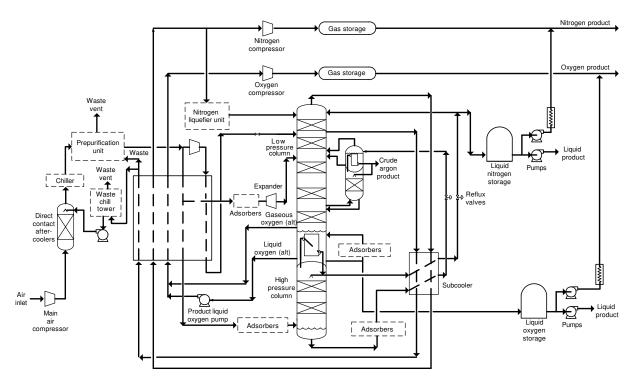


Figure 1—Representative air separation plant flow diagram

Oxygen has the highest boiling point of the three main components and is taken from the bottom of the LP column. Nitrogen is taken from the top of the LP or HP columns. An argon-rich stream can be withdrawn from the middle of the LP column and refined to a pure product in other distillation columns. The product streams are warmed to ambient temperature against incoming air in the main heat exchanger to recover the refrigeration. It is also possible to remove the products from the distillation system as liquid, if sufficient refrigeration is available. Producing large quantities of liquid products requires extra refrigeration, often supplied by a nitrogen liquefier unit. Liquid may be stored for pipeline backup or merchant sales.

There are two typical ASU configurations for producing pressurized oxygen. In the gas plant configuration (also called gaseous oxygen [GOX] process or classic gas process), oxygen is taken as a vapor from the bottom of the LP column and warmed by incoming air in the main heat exchanger. If an HP oxygen product is needed, it is compressed to the required pressure. A LOX purge stream is taken from the sump of the LP column to prevent the trace contaminants from concentrating above allowable safety limits. In the pumped LOX process (also known as the internal compression process), oxygen is taken as a liquid from the LP column sump, pumped to the required pressure, and vaporized in the main exchanger against HP air from the booster air compressor. The pumped oxygen stream removes trace contaminants from the LP column sump, so a separate LOX purge stream from the LP column sump may be eliminated.

There are many other configurations of the ASU process that are specifically tailored for different products mixes and customer needs. A detailed discussion of these is beyond the scope of this publication.

## 4 Definitions

## 4.1 Publication terminology

#### 4.1.1 Shall

Indicates that the procedure is mandatory. It is used wherever the criterion for conformance to specific recommendations allows no deviation.

### 4.1.2 Should

Indicates that a procedure is recommended.

### 4.1.3 May

Indicates that the procedure is optional.

#### 4.1.4 Can

Indicates a possibility or ability.

### 4.2 Acid gas

Air contaminants such as chlorine, NO<sub>x</sub>, and SO<sub>x</sub> that can form acid when combined with water.

NOTE—Acid gases can create corrosive conditions in brazed aluminum heat exchangers (BAHXs) and other equipment.

#### 4.3 Adsorption

Purification process in which one or more components from a gas or liquid is preferentially adsorbed onto a solid desiccant or other adsorbent.

NOTE—Typical adsorbents include:

- Molecular sieve—granular adsorbent (typically 13X) used in air PPUs for water, carbon dioxide, and hydrocarbon removal;
- Alumina—granular adsorbent typically used in air PPUs or dryers for water removal; and
- Silica gel—granular adsorbent typically used in cryogenic adsorbers for carbon dioxide and hydrocarbon removal.

#### 4.4 Asphyxiation

To become unconscious or die from lack of oxygen.

### 4.5 Blow out

Maintenance or commissioning procedure in which a fluid, typically dry air, is blown through piping and equipment to eliminate dirt, moisture, or other contaminants.

### 4.6 Brazed aluminum heat exchanger (BAHX)

An aluminum plate and fin heat exchanger consisting of corrugated sheets separated by parting sheets and an outer frame consisting of bars with openings for the inlets and outlets of fluids, equipped with headers and nozzles to connect to external piping.

NOTE—The approximate thickness of the corrugated sheets is 0.2 mm to 0.5 mm, while the parting sheets have thicknesses between 1.0 mm and 2.4 mm. More information is provided in CGA G-4.9, Safe Use of Brazed Aluminum Heat Exchangers for Producing Pressurized Oxygen [2].

### 4.7 Casing

Outside walls of a coldbox or cryogenic piping duct. The cross section can be circular or rectangular.

### 4.8 Catalyst

Material that helps promote a reaction but is not changed itself.

#### 4.9 Cavitation

This phenomenon occurs when the pressure of a liquid drops below the vapor pressure of the liquid at a certain temperature. At this point, liquid will vaporize, thereby creating vapor bubble. These bubbles can cause a pump to lose prime or suffer heavy vibration and damage.

# 4.10 Centrifugal

Dynamic compressor or pump that works by accelerating a fluid in a rotating impeller with subsequent conversion of this energy into pressure.

#### 4.11 Cleanup

Removing trace contaminants from a stream or from process equipment.

#### 4.12 Coldbox

Structure that contains cryogenic distillation columns, other process equipment, piping, and insulation; can also refer to the cryogenic portion of an ASU.

### 4.13 Control system

System that responds to input signals from the process, operator, or both and generates an output that causes the process to operate in the intended manner.

## 4.14 Crude argon purification system

Warm equipment including compressors, catalytic reactors, heat exchangers, driers, and chillers used for removing oxygen from crude argon.

## 4.15 Cryogenic liquid

Liquid that is extremely cold, less than -130 °F (-90 °C).

### 4.16 Dead end boiling (pool boiling, pot boiling)

The condition occurring in thermosyphon reboilers where, due to blockages, the flow of liquid is restricted within the channels of the reboiler, thereby reducing the removal of contaminants by the flushing action of the liquid. Also known as pool or pot boiling. This phenomenon can also occur in cavities and sections of piping where oxygen-enriched liquid can be trapped and vaporized by heat leak.

NOTE—This process is particularly hazardous when the oxygen-enriched liquid contains hydrocarbons that become concentrated during vaporization.

### 4.17 Differential temperature ( $\Delta T$ )

Temperature difference between two streams in a heat exchanger, which is an indicator of the exchanger's performance and efficiency.

### 4.18 Deriming

Periodic preventive maintenance procedure where the process equipment is warmed up while simultaneously being swept with clean dry gas to remove any accumulated moisture, carbon dioxide, and atmospheric contaminants.

NOTE—Also known as defrosting, de-icing, and thawing.

#### 4.19 Deoxidation or deoxo

Catalytic removal of trace oxygen contaminant from a gas by a reaction with hydrogen, <u>typically in warm argon production in ASUs.</u>

### 4.20 Deoxo systems

Catalytic-based system used in <u>some</u> argon refining <u>systems to remove</u> oxygen. Hydrogen is added to the crude argon stream and then reacts with oxygen to form water.

## 4.21 Distance piece

Extended spacer, <u>intermediate support</u>, <u>or carrier frame</u> that isolates the process end of a pump or compressor from its motor or bearings to prevent migration of process fluid, oil, heat, or refrigeration.

## 4.22 Double block and bleed

Piping or instrument arrangement that combines two block (or isolation) valves in series with a vent valve in between the block valves as a means of releasing pressure between the block valves with the intent to provide positive isolation.